SSPMA

Sump and Sewage Pump Manufacturers Association

Since 1956, we are a North American trade organization of sump, effluent, and sewage pump manufacturers and their suppliers.

Working together to:

- □ train wastewater and plumbing professionals, and
- □ create product performance and safety standards.

SSPMA members collaborate with each other and government regulators to educate consumers and professionals on the latest products, their application, proper sizing techniques, safe installation and use, and good maintenance practices.



Pumps bearing the "SSPMA-Certified" seal have been tested by the member manufacturer in accordance with SSPMA Industry Standards.



The Standards are designed to provide accurate performance data for sump, effluent and sewage pumping equipment, to assist in their proper application and selection.



SSPMA MEMBERS

Barnes Pumps / Crane Pumps & Systems Champion Pump Company, Inc.

Eco-Flo Products Inc. / Ashland Pump Company

Franklin Electric / Little Giant Glentronics, Inc.

Goulds Water Technology, a xylem brand

Liberty Pumps

Pentair Water





SSPMA ASSOCIATE MEMBERS

Alderon Industries
John Crane, Inc.
SJE-Rhombus
Topp Industries, Inc.



FOR SUMP, EFFLUENT AND SEWAGE PUMPS

RECOMMENDED STANDARDS



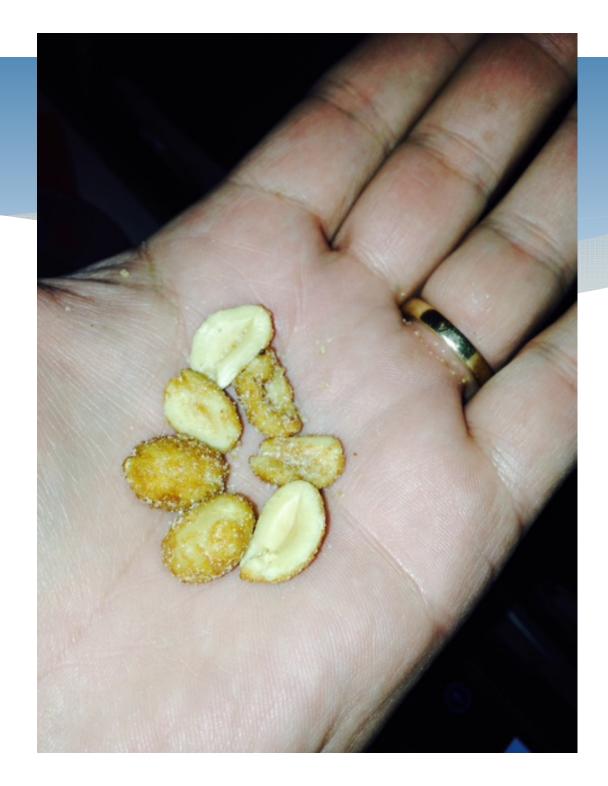


SUMP & SEWAGE PUMP MANUFACTURERS ASSOCIATION • P.O. BOX 647 • NORTHBROOK, IL 60065-0647













1/2HP Sewage

0	Type	Model #	HP	RPM	Dia a	Callala	A t	0	TDII	401	001	201	401	VACT
Company	Туре	Woder #			Disc.	Solids	-		TDH	10'	20'	30'	40'	WT.
			1/2	1750	2	2	Υ	15	25	115	45			62
			1/2	1750	2	2	Υ	15	26	140	50			84
			1/2	1750	2	2	N	15	27	130	65			75
			1/2	3450	2	2	N	15	39	80	80	50		80
			1/2	3450	2	2	Υ	10	26	100	45			38
	DN		1/2	3450	2	2	N	20	40	105	100	45		75
			1/2	3400	2	2.00	Υ	20	27	105	40			31
			1/2	1750	2	1.50	N	20	26	110	40			70
			1/2	1750	2	2.00	N	20	27	124	52			76
			1/2	3500	2	2.00	N	20	30	110	62			65
			1/2	1750	2	2.00	Υ		18	62				23
			1/2	1750	2	2.00	Υ	10	28	130	70			62
			1/2	1750	2	2.00	Υ	10	20	160				53
			1/2	1750	2	2.00	Υ	10	24	110	30			55
			1/2	3450	2	2.00	N	20	44		124	69	16	76
			1/2	1750	2	2	Υ	10	24	110	40			42
			1/2	1750	2	2.00	Υ	10	20	85				46
			1/2	1750	2	1.25	Υ	15	28	100	50			41
			1/2	1750	2	2.00	N	20	24	100	35			87
			1/2	1750	2	2.00	Υ	20	18	60				32
			1/2	1750	2	2.00	Υ	20	23	110	40			76
			1/2	1750	2	2.00	Υ	20	27	130	65			42
			1/2	3450	2	2.00	N	20	37	125	99	40		84
			1/2	3450	2	1.50	N	20	41	90	68	38	5	75
			1/2	1750	2	2.00	Υ	10	21	89	10			41
			1/2	1750	2	2.00	Υ	10	26	85	38			50
			1/2	1750	2	2.00	Υ	10	21	89	10			51
			1/2	1750	2	2.00	Υ	10	26	95	33			83
			1/2	3450	2	2.00	N	20	39	116	83	46		86

Sump Pump



A pump powered by an electric motor for the removal of clear and/or ground water drainage from a sump, pit or low point in a residential, commercial or industrial property.

(Less than ½" Solids)

Effluent Pump



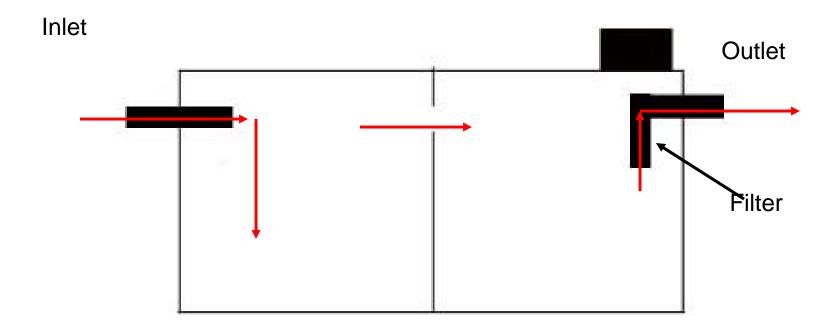
A pump powered by an electric motor for the removal of natural or artificial pretreated liquid waste discharge from an onsite sewage treatment system.

(½" To Less Than 1" Solids)



Everybody Know What Effluent Is?

Septic Tank Effluent





Should an effluent pump be able to pass solids?

What is the difference between a sump pump and an effluent pump?

Sewage Pump



A pump powered by an electric motor for the removal of wastewater from a sealed basin containing solids of up to 2" in diameter.

(1" Through 2" Solids)

Sewage Pump



Why should a sewage pump be able to pass 1 to 2" Solids?

Sewage Pump



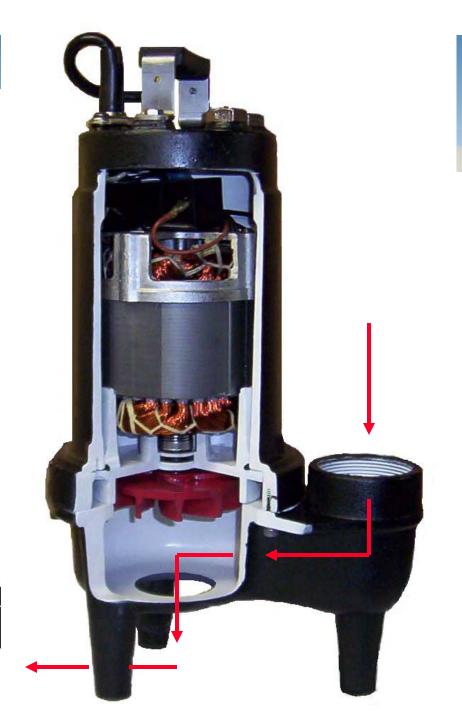
Can you use a sewage pump as a sump or effluent pump?

Can you use a sump or effluent pump as a sewage pump?

SSPMA



A solid is a sphere of a stated size, plus 0.00 or minus 0.02 on the diameter, that will freely pass through the strainer and inlet of the pump or the inlet of the pump with no strainer, through or under the impeller vanes or a combination of both without interference with the surrounding volute housing, and out the discharge opening.





SSPMA

(c) All readings shall be referenced to the centerline of pump on horizontal pumps, and to the entrance eye of the first stage impeller on vertical units.

5. Capacity:

Capacity will be measured in U. S. gallons per hour or per minute or liters per hour or per minute.

6. Static Sphere Size Test:

A sphere as described in the definition and made of steel is to be placed in the discharge of a pump and must freely pass from the outlet to the inlet and out the strainer if present with the pump not running. The pump may be moved from the normally installed position only enough to allow the sphere to roll to the inlet and out the strainer if present. The pump orientation from the normally installed position may be changed during the test only if doing so will not increase the clearance between the volute housing and case. The pump shaft may be rotated by hand during the test.

7. Power:

Pump shall be tested at nameplate voltage rating. Power will be measured as brake horsepower input to the pump.

8. Test Setup:

- (a) Test shall be conducted using clear water at temperatures between 50° F (10° C) and 80° F (27° C).
- (b) The liquid around the pump shall be relatively quiet and not filled with entrained air whirls, etc., from recirculated discharge.
- (c) Manometer lines, if used, shall be arranged for venting to keep them full of water.

9. Test Procedure:

- (a) The test shall not be conducted until test conditions have stabilized.
- (b) Sufficient observations shall be made from 0 to maximum capacity to define the characteristics.

10. Rating:

- (a) The pumps covered by this Standard shall be rated as capable of delivering a stated capacity in U. S. gallons per hour or gallons per minute, at a stated head in feet, or liters per hour or liters per minute, at a standard head in meters, based on sea level performance.
- (b) It is recommended that total head be listed in increments of 5 feet starting at 5 feet and/or the metric equivalent (1.524 meters).
- (c) Solids-handling capability of pumps will be stated in inches and metric in parenthesis.

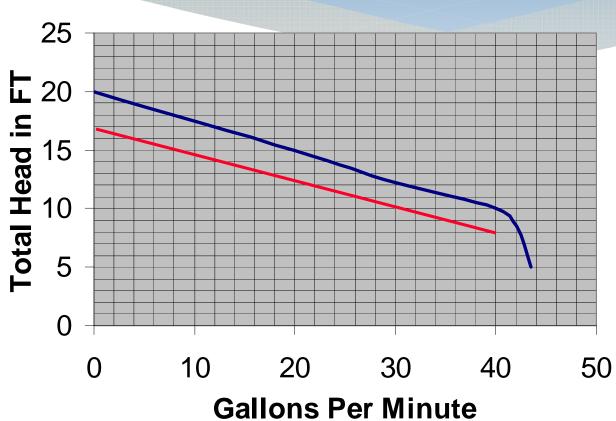
11. Tolerances:

The capacity of any new production pump shall not be less than 90 percent of rated capacity at stated total heads.



Curves (20GPM@15'TDH)





Pumps & Types of Construction



Brass or Bronze

Cast Iron

Aluminum

Plastic

Stainless Steel

Motors



Oil filled / Air filled

Shaded Pole

Split Phase

Permanent Split Capacitor

Capacitor Start Capacitor Run

Motors



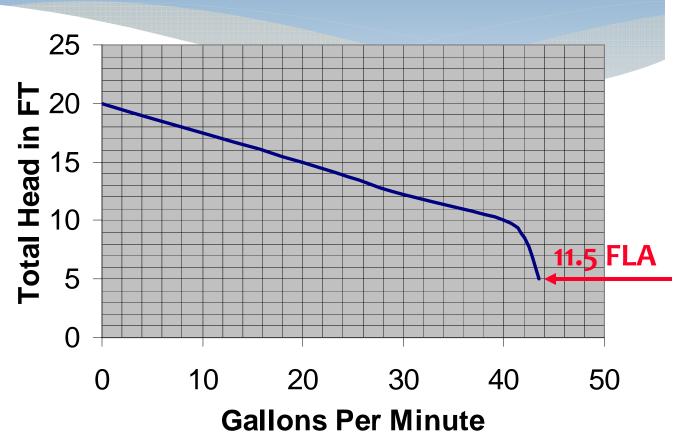
	Shaded Pole	Split Phase	Permanent Split Capacitor	Capacitor Start Capacitor Run		
Starting Switch	No	Yes	No	Yes		
Starting Torque	Low	Low	Low	High		
Efficiency	Low	Medium	High	High		

What is Thermal Overload Protection?



What Is Full Load Amps?





Full Load Amps



PUMP A 4.0

PUMP B 5.2

PUMP C 8.0

PUMP D 9.7

Motors



Service Life of Electrical Equipment Diminishes by Approximately Half For Every 10 Degrees C Temperature Increase

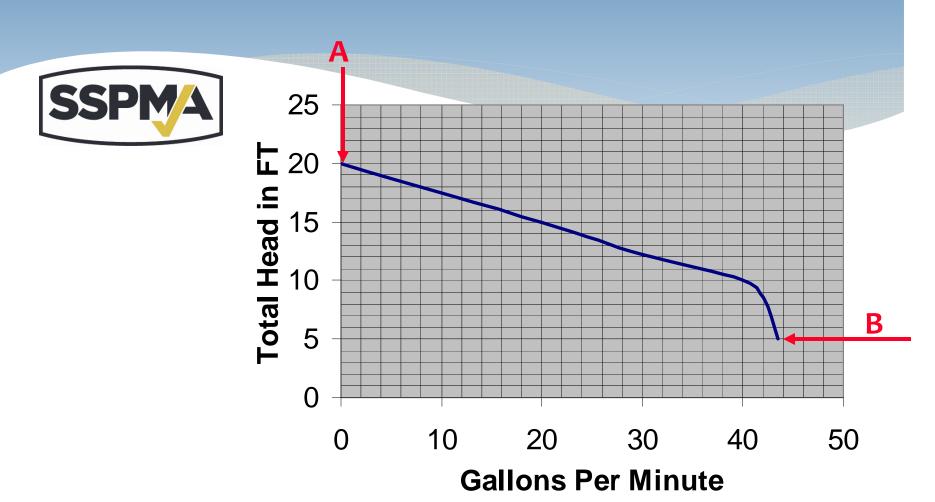
Motors



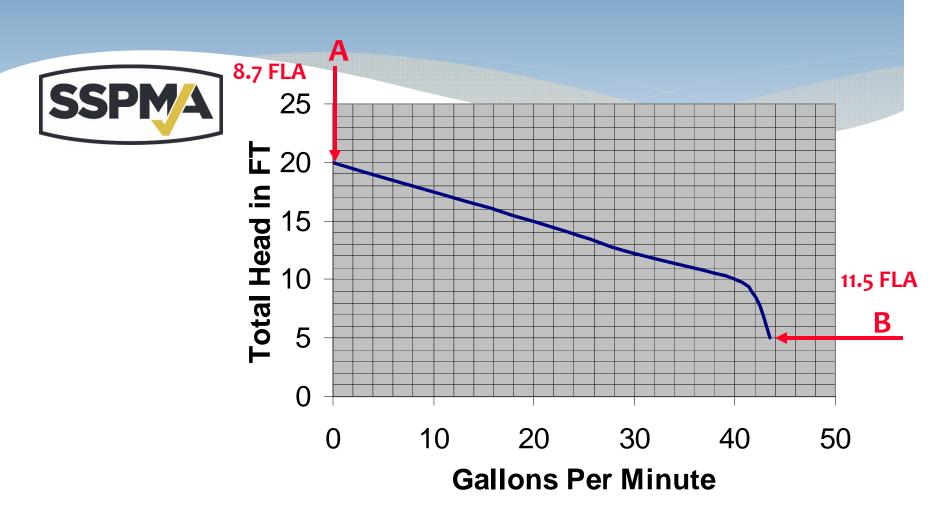
Designed to last 10 years at 100 deg. c.

Will only last 5 years at 105 deg. c.

Where Does The Pump Work The Hardest? A or B



Where Does The Pump Work The Hardest? A or B



Power Cords



SJOOW

SJ= Junior Duty 300 Volts

O= Oil Resistant Outer Jacket

OO= Oil Resistant Outer Jacket & Insulation

W= Weather & Water Resistant

T= Thermoplastic Jacket

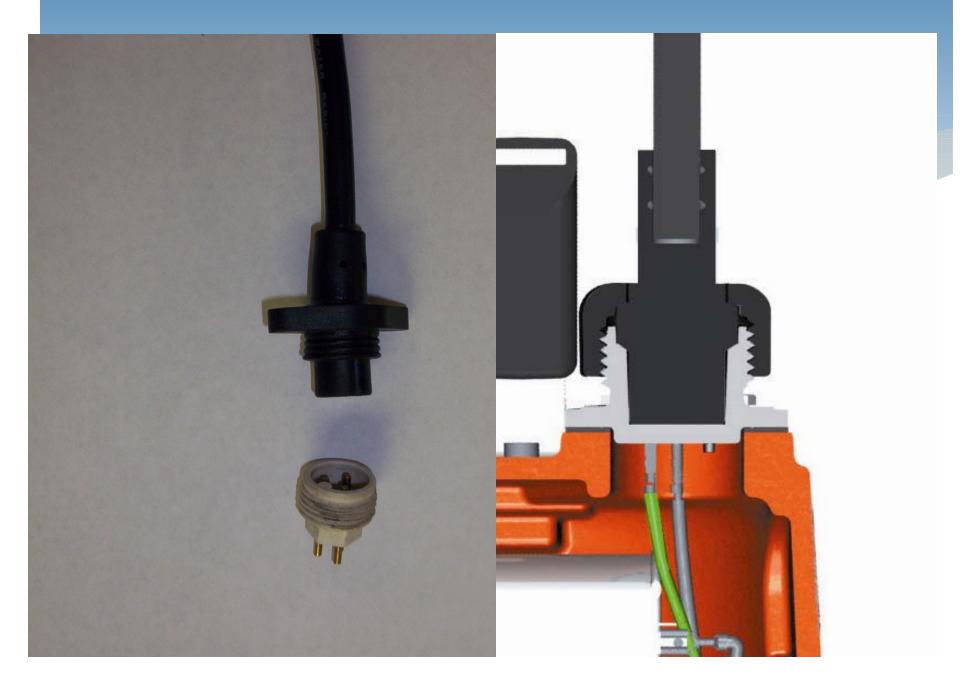
Power Cords



Power Cords Entrances



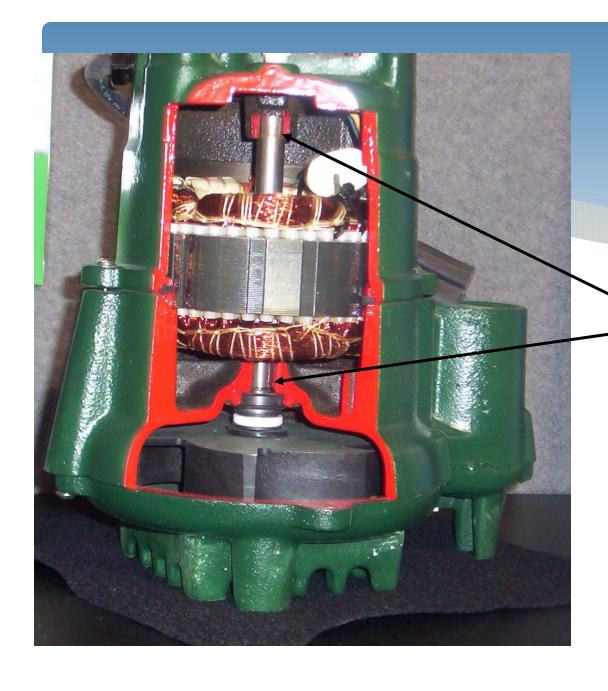
Power Cords Entrances



Bearings



Sleeve Ball



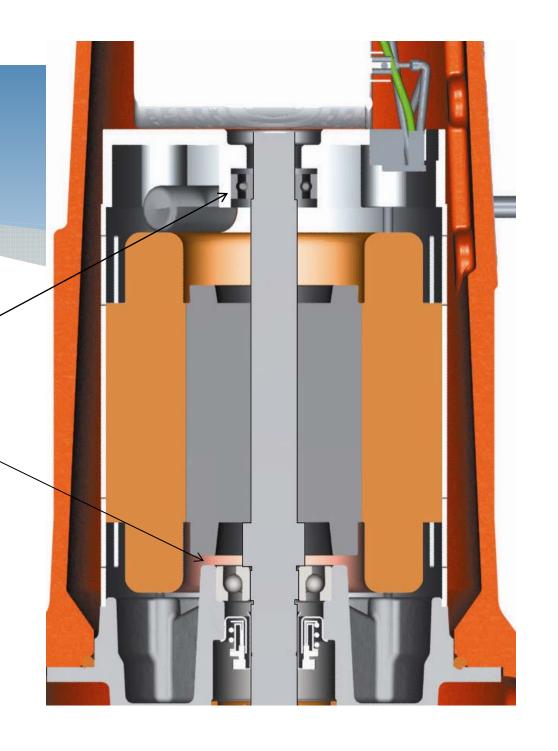
Sleeve Bearings







Upper & Lower Ball Bearings



Impellers



- * Plastic
- * Cast Iron
- * Brass
- * Stainless Steel
- * Aluminum

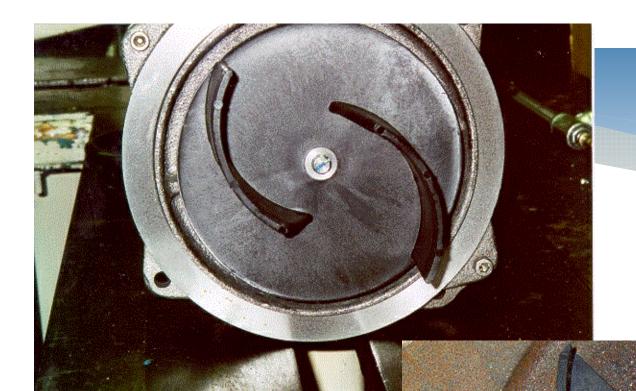
- * Vortex
- * Non-Clog
- * Enclosed
- * Single Vane

Vortex

Non Clog











Seals



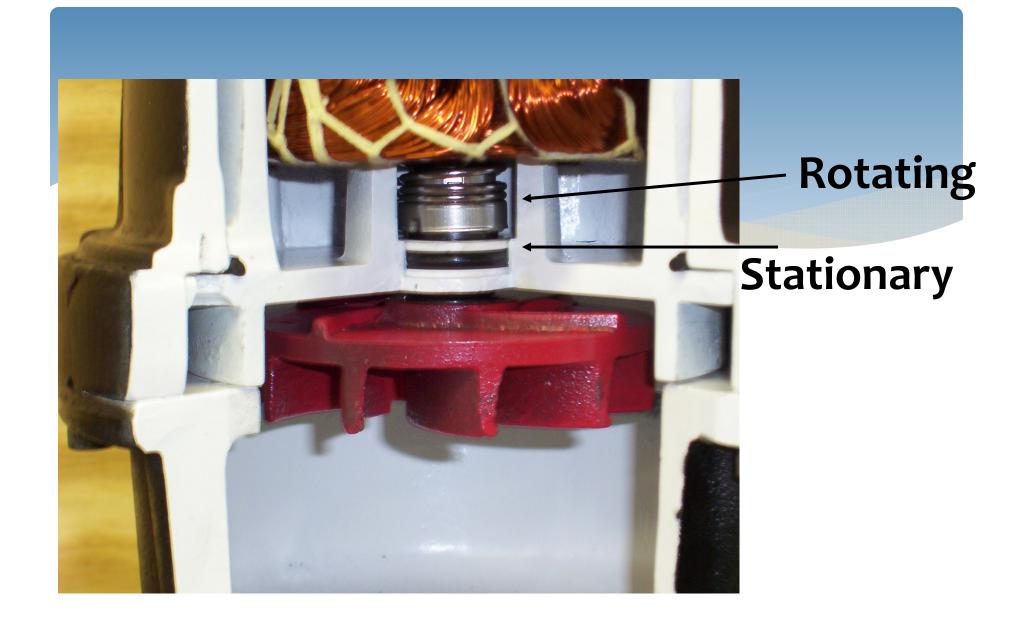
Carbon

Silicon

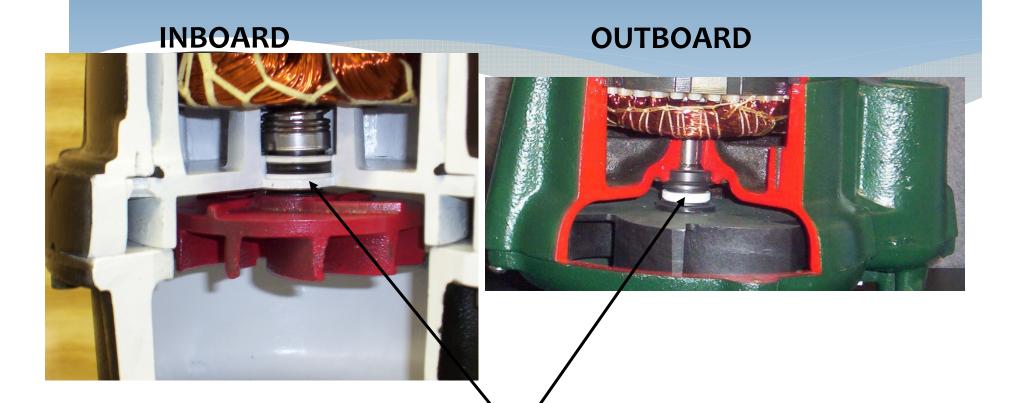
Tungsten

Seals

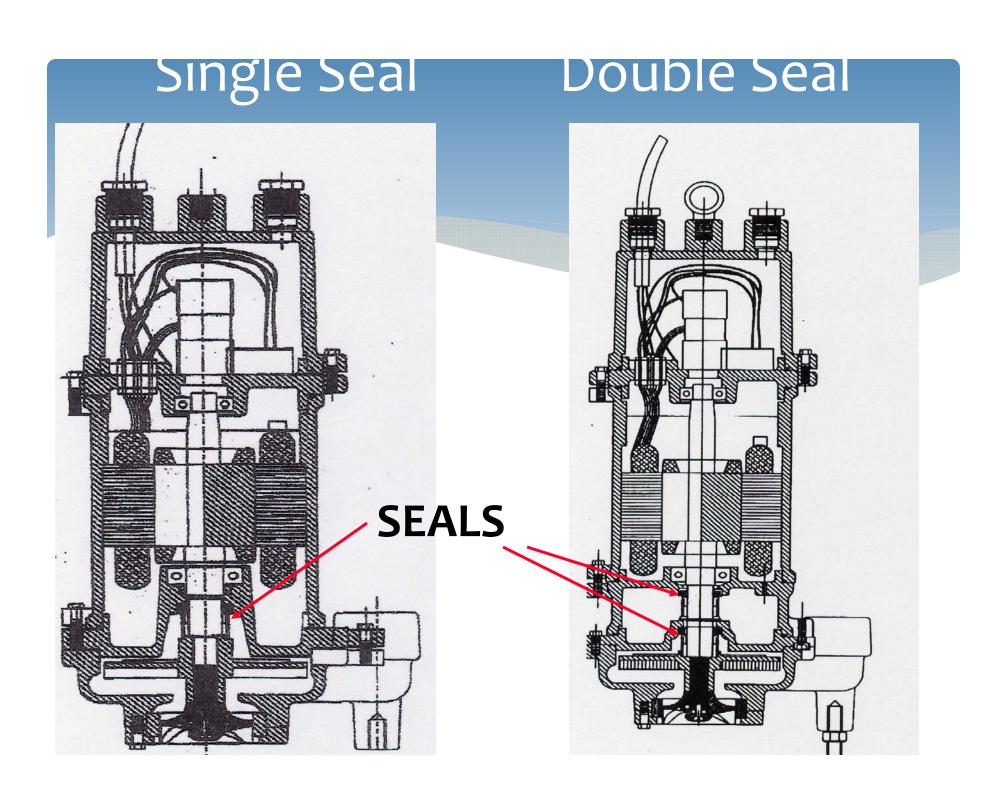




Seals



Sealing Area





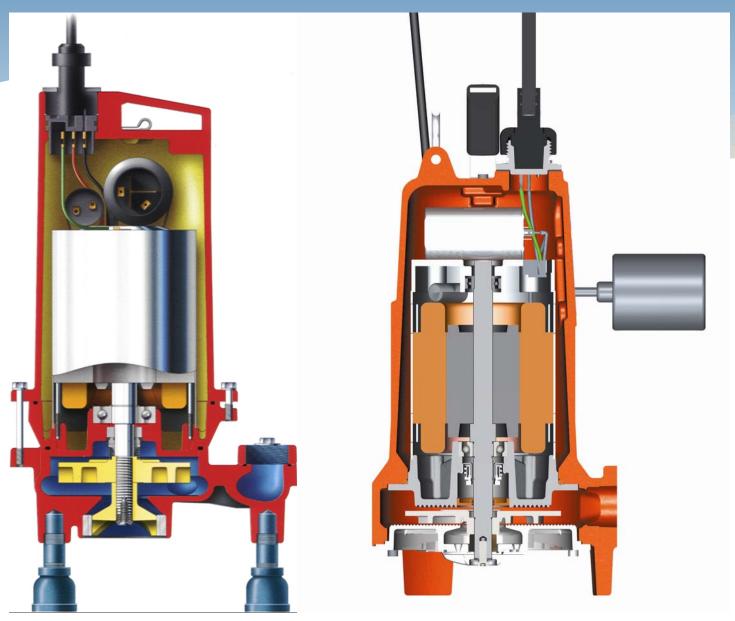
* What is the difference between a Grinder Pump and a Sewage Ejector?



- * A Grinder Pump cuts the sewage into a slurry before pumping it.
- * A Sewage ejector pumps the solids



* Never need a grinder pump to pump effluent from a septic tank to a leach field.











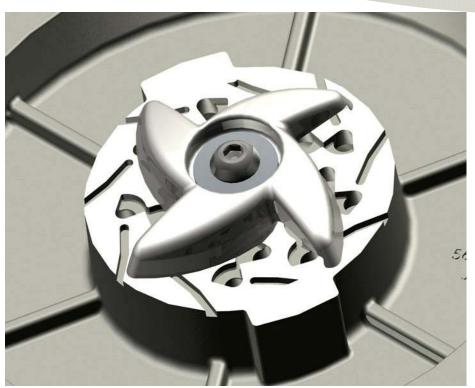




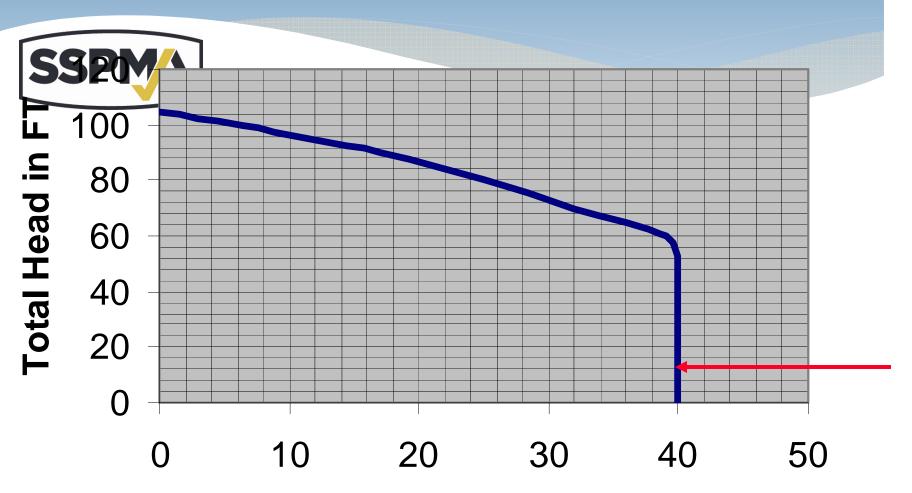






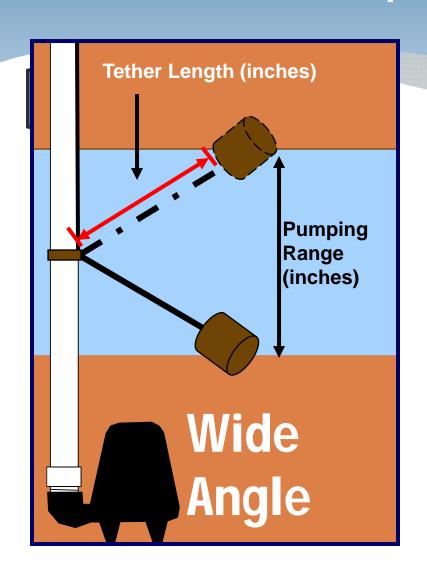


PUMP PERFORMANCE CURVE



Gallons Per Minute

Pump Switch

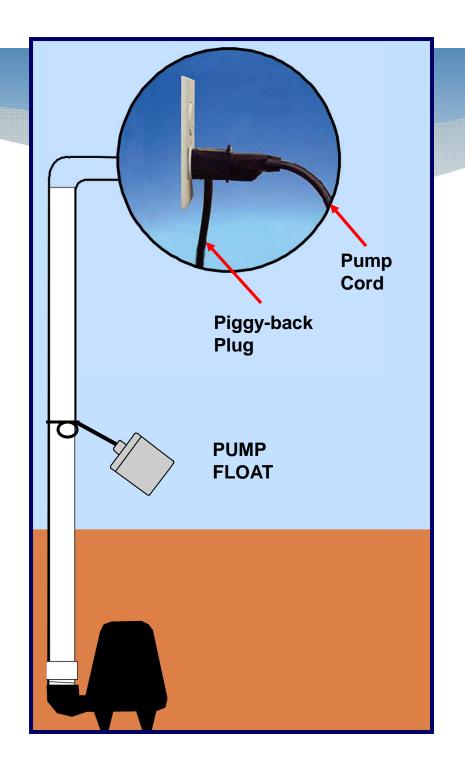


Tether Length	Pumping Range
3.5	6.6
6	8.5
8	11
10	13
12	14
15	17
17	19

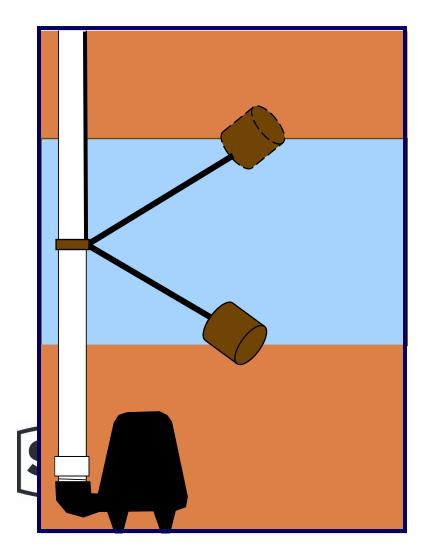
Pump Switch

Piggy-back plug option





Pump Switch



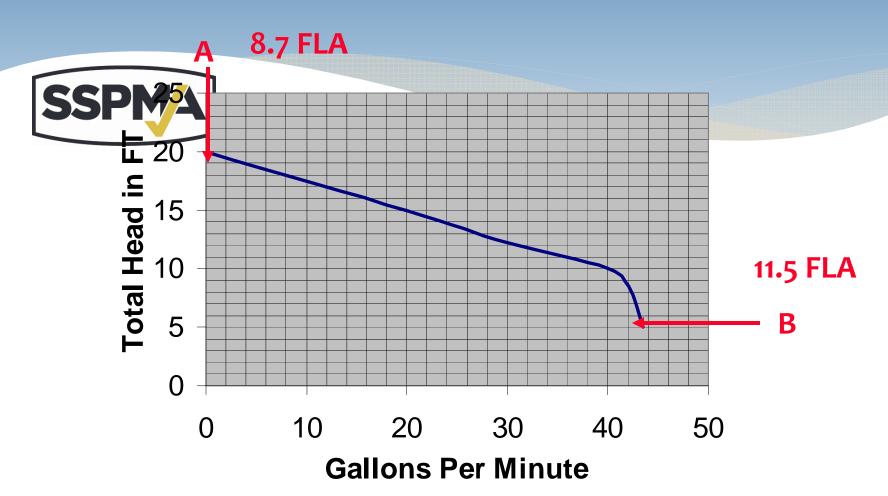
The Best
Location For A
Switch Is For
The Pump To
Always Be
Submerged!



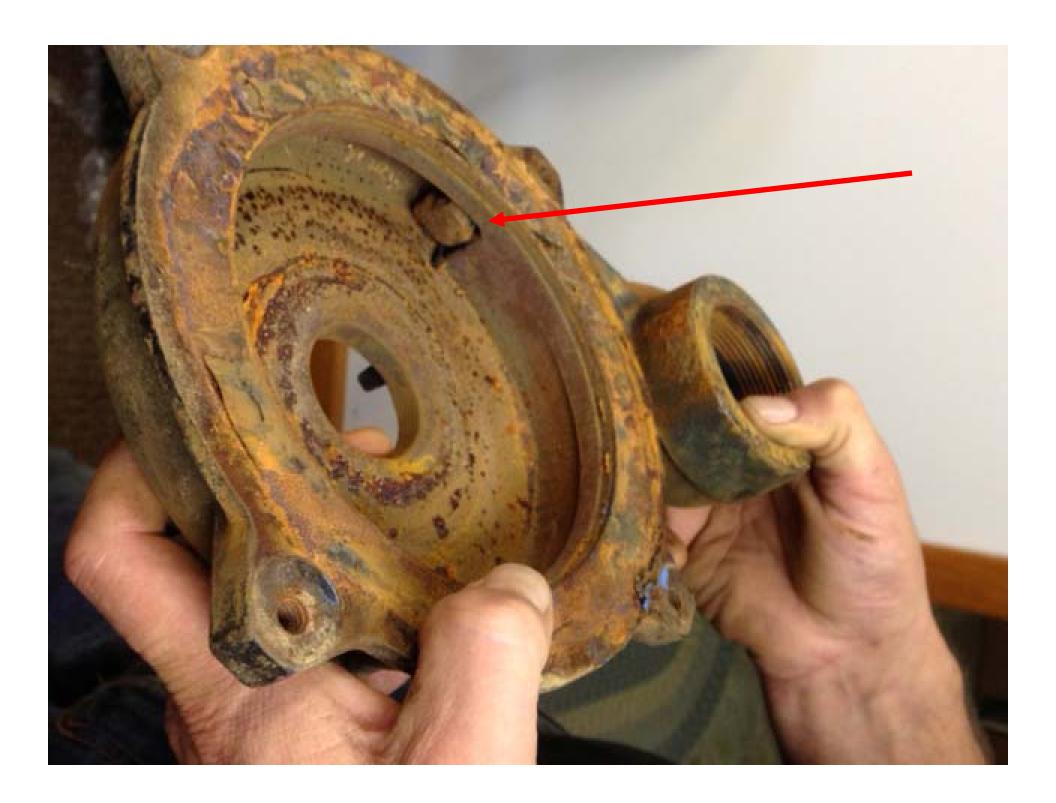
What Are Some Reasons Pumps Might Not Work?



- * Pump Sized Correctly
- * Switch Or Control Failure
- Check Amps
- * Low or Incorrect Voltage
- Tripped Thermal Sensor
- * Debris In Volute
- * Volute Inlet Blocked
- Discharge Line Could Be Blocked
- * Check Valve Could Be Bad
- Pump Could be Air Locked







FOR NEW OR REPLACEMENT **EFFLUENT PUMPS**

RECOMMENDED
GUIDELINES FOR
SIZING EFFLUENT PUMPS



Effluent Pump Sizing & Selection



SIZING GUIDELINES

SUMP AND SEWAGE PUMP MANUFACTURERS ASSOCIATION

SSPMA° Certified

Sewage Pump Sizing & Selection

Sewage Pump Sizing & Selection



Top Questions



If somebody wants to size a pump, what do they need to know?

Top Questions



- * Pump Capacity Requirements (GPM)
- * Solids Handling Requirements
- * Discharge Piping Diameter Preferred
- * Voltage & Phase Requirements
- * Total Dynamic Head (TDH) Of The Installation
 - * What Is The Static Head
 - * What Is The Length Of The Discharge Piping

Top Questions



- * Is There A Control Panel Required
 - * Simplex Or Duplex System
- * Is There A Break A Way System Required
- * Basin (Sump) Size

Total fixture units from Fig. "A" w	ork sheet				{	[1]		
GPM requirements from Fig. "B"					{	[2]	GPM	
Pipe Size				.{3}				
Friction factors from Fig. "D"	Factor	Qty.	Total					
90 Deg. bends								
45 Deg. bends								
Tee (thru-flow)								
Tee (branch flow)								
Swing check valve Gate valve								
Disch. Pipe length				{4 }				
<u> Dison. 1 ipe lengui</u>				ניין				
Systems' total feet o	f piping			{5 }				
Friction head per / 100' of pipe from				.{6}				
Multiplied by the number of 100' of total system piping to determine Head.			Friction He Static Hea			7} 8}		
			TDH		{	9}	TDH	

Pump Capacity Requirements



Pump capacity refers to the rate of flow in GPM which is necessary to efficiently maintain the system

- * List all fixtures involved in the installation.
- * Using figure A", worksheet, assign a fixture unit value to each.
- * Determine the total fixture units. {1}

SSPMA FIGURE "A"

Fixture Description	Fixture Unit Value	Fixture Description	Fixture Unit Value
Bathtub, 1-1/2" trap	2	Sink, service type	3
Bathtub, 2" trap	3	Sink, scullery	4
Bidet, 1-1/2" trap	3	Sink, surgeons	3
Dental unit or cuspidor	1	Swimming pool (per 1000) gal.)	1
Drinking fountain	1	Urinal	4**
Dishwasher, domestic	2	Washing machine	2
Kitchen sink	2	Water closet	3**
Kitchen sink with disposal	3	Water Softener	4
Lavatory, 1-1/2" trap	1	Unlisted fixture, 1-1/4" trap	2
Lavatory, barber/beautician	2	Unlisted fixture, 1-1/2" trap	3
Laundry tray	2	Unlisted fixture, 2" trap	4
Shower	2	Unlisted fixture, 2-1/2" trap	5
Shower, group (per head)	3	Unlisted fixture, 3" trap	6
Bathroom group consisting of lav	zatory, bathtu	b or shower, and water closet	6**

^{**} Add 4 fixture units for each flush valve fixture.

Pump Sizing Example #1



- * Four Bathrooms
- * Dishwasher
- Washing Machine
- Laundry Tray
- * Water Softener

- * Kitchen Sink with Disposal.
- * Basement Shower
- * 13,000 Gallon Pool
- * Bar Sink (1-1/2" Trap)

FIGURE "A" WORKSHEET

Fixture Description	Fixture Unit	Qty.	Sub. Total	Fixture Description	Fixture Unit	Qty.	Sub. Total
•	Value		Units	-	Value		Units
Bathtub, 1-1/2" trap	2			Sink, service type	3		
Bathtub, 2" trap	3			Sink, scullery	4		
Bidet, 1-1/2" trap	3			Sink, surgeons	3		
Dental unit or cuspidor	1			Swimming pool (per 1000) gal.)	1	13	13
Drinking fountain	1			Urinal	4**		
Dishwasher, domestic	2	1	2	Washing machine	2	1	2
Kitchen sink	2			Water closet	3**		
Kitchen sink with disposal	3	1	3	Water Softener	4	1	4
Lavatory, 1-1/2" trap	1			Unlisted fixture, 1-1/4" trap	2		
Lavatory, barber/beautician	2			Unlisted fixture, 1-1/2" trap	3	1	3
Laundry tray	2	1	2	Unlisted fixture, 2" trap	4		
Shower	2	1	2	Unlisted fixture, 2-1/2" trap	5		
Shower, group (per head)	3		_	Unlisted fixture, 3" trap	6		_
Bathroom group consisting of la	water closet	6**	4	24			
** Add 4 fixture units for each flush valve	fixture.			TOTAL FIXTURE UNITS			55

Total fixture units from Fig. "A" work sheet	55 {1}			
GPM requirements from Fig. "B"	{2}	GPM		
Pipe Size		{3}		
Friction factors from Fig. "D" Factor	Qty. To	tal		
90 Deg. bends				
45 Deg. bends				
Tee (thru-flow)				
Tee (branch flow)				
Swing check valve				
Gate valve				
Disch. Pipe length		{4}		
Systems' total feet of piping		{5}		
Friction head per / 100' of pipe from Fig. "E"		<u></u> {6}		
Multiplied by the number of 100' increments of total system piping to determine Friction Head.		on Head Head	{{7}} {{8}}	
	TDH		 {9}	TDH

Pump Capacity Requirements

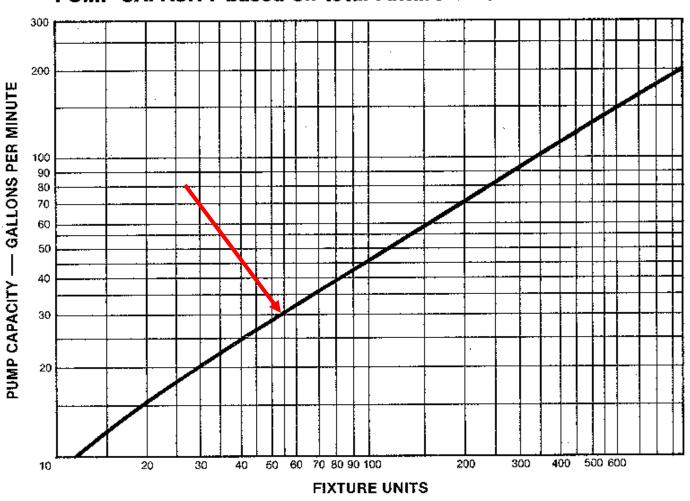


Pump capacity refers to the rate of flow in GPM which is necessary to efficiently maintain the system

- * List all fixtures involved in the installation.
- * Using Figure"A", Worksheet, assign a fixture unit value to each.
- * Determine the total fixture units. {1}
- * Use figure "B" and determine the PUMP CAPACITY in GPM. {2}

SSPMA FIGURE "B"

PUMP CAPACITY based on total Fixture Units



SSPMA FIGURE "B"



In order to endure sufficient fluid velocity to carry solids (which is generally accepted to be 2 feet per second), the following are minimum required flows

- 21 GPM through 2" pipe
- 46 GPM through 3" pipe
- 78 GPM through 4" pipe

Total fixture units from Fig. "A" wo	rk sheet				55{1}		
GPM requirements from Fig. "B" .	30 {2}	GPM	30				
Pipe Size				_{3}			
Friction factors from Fig. "D"	Factor	Qty.	Total	_			
90 Deg. bends							
45 Deg. bends							
Tee (thru-flow)							
Tee (branch flow)							
Swing check valve							
Gate valve							
Disch. Pipe length				{4}			
Systems' total feet of	piping			{5 }			
Friction head per / 100' of pipe from	m Fig. "E"		·	_{6}			
Multiplied by the number of 100' in of total system piping to determine Head.			Friction Hea		{{7}} {{8}}		
			TDH			TDH	

Total Dynamic Head (TDH)



TDH is a combination of two components- Static Head and Friction Head- and is expressed in feet.

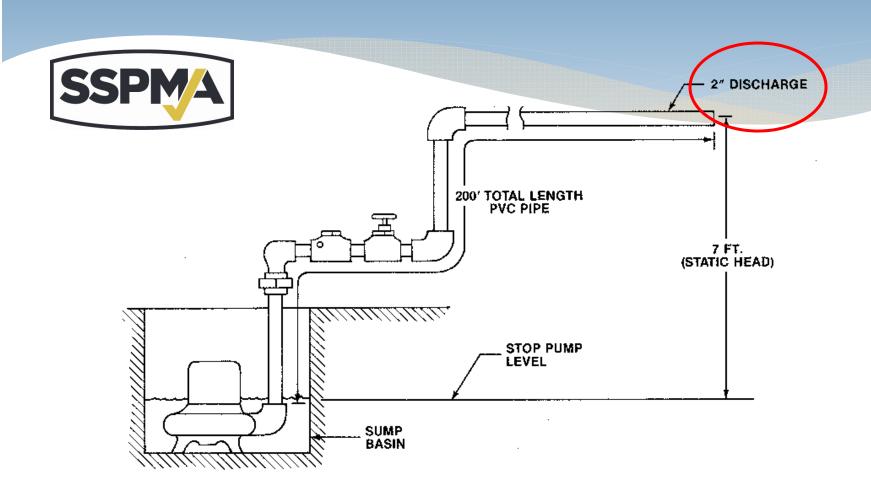
- * Static Head is the actual vertical distance measured from the minimum water level in the basin to the highest point in the discharge piping.
- * Friction Head is the additional head created in the discharge system due to resistance to flow within its components.

Total Dynamic Head (TDH)



* Determine discharge piping size {3}.

SSPMA FIGURE "C"



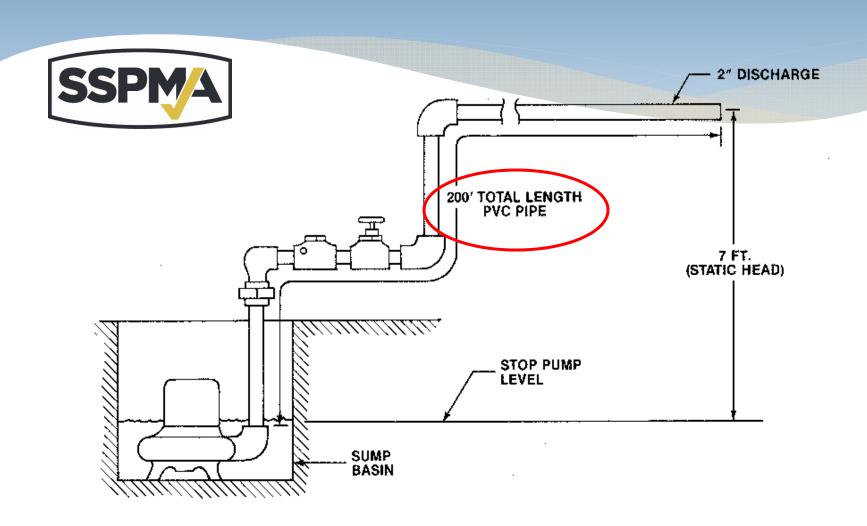
Total fixture units from Fig. "A" wo		55	_{1}					
GPM requirements from Fig. "B"						_{2}	GPM	30
Pipe Size			2"	{3}				
Friction factors from Fig. "D"	Factor	Qty.	Total	_				
90 Deg. bends								
45 Deg. bends								
Tee (thru-flow)								
Tee (branch flow)								
Swing check valve								
Gate valve								
Disch. Pipe length				{4}				
0. 1			1	 (5)				
Systems' total feet of	piping			_ {5}				
Friction head per / 100' of pipe fro	m Fig. "E"			_{6}				
Multiplied by the number of 100' in of total system piping to determine Head.			Friction H Static Hea			_{7} _{8}		
			TDH			= {9}	TDH	

Total Dynamic Head (TDH)



- * Determine discharge piping size {3}.
- Determine length of discharge piping {4}.

SSPMA FIGURE "C"



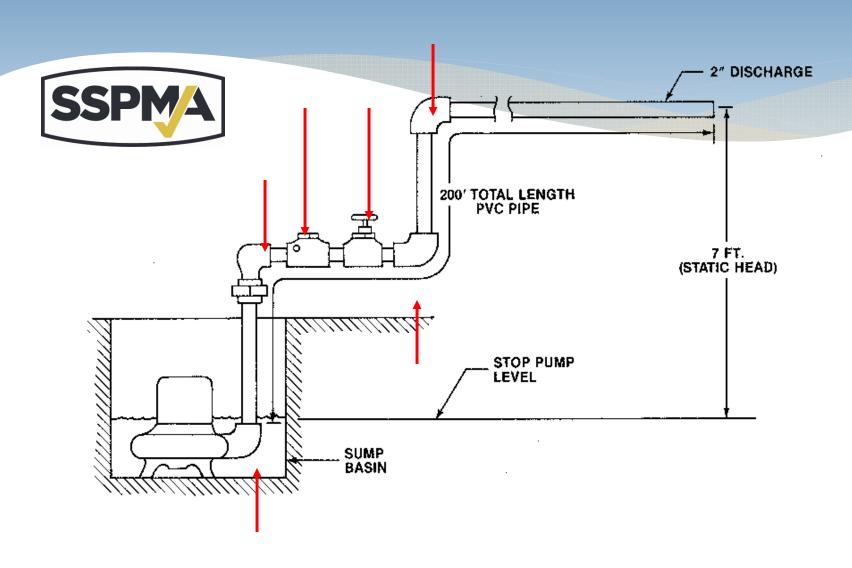
Total fixtu	re units from Fig. "A" w	ork sheet .		55	_{1}				
GPM requ	irements from Fig. "B"			30	2	GPM	30		
Pipe Size				2"	_{3}				
Friction fa	ctors from Fig. "D"	Factor	Qty.	Total	_				
	90 Deg. bends				_				
	45 Deg. bends				4				
	Tee (thru-flow) Tee (branch flow)				\dashv				
	Swing check valve				4				
	Gate valve				₫				
	Disch. Pipe length			200'	4 }				
					<u> </u>				
	Systems' total feet of	f piping			{5}				
Friction he	ead per / 100' of pipe fro	om Fig. "E"			_{6}				
•	by the number of 100' i stem piping to determin			Friction H Static Hea			-{7} -{8}		
i icau.				TDH			= {9}	TDH	

Total Dynamic Head (TDH)



- * Determine discharge piping size {3}.
- * Determine length of discharge piping {4}.
- * List all fittings and multiply by their factor, Figure "D". Add to length of discharge piping {4} to determine systems total feet of piping {5}.

SSPMA FIGURE "C"



Total fixture units from Fig. "A" w	ork sheet	55	_{1}					
GPM requirements from Fig. "B"	30	{2}	GPM	30				
Pipe Size			2"	_{3}				
Friction factors from Fig. "D"	Factor	Qty.	Total					
90 Deg. bends		3						
45 Deg. bends								
Tee (thru-flow)				_				
Tee (branch flow) Swing check valve		1		-				
Gate valve		1		-				
Disch. Pipe length		,	200'	{4}				
Systems' total feet o	 of piping			- {5}				
Friction head per / 100' of pipe from	om Fig. "E"			_{6}				
Multiplied by the number of 100' of total system piping to determine Head.			Friction F Static He			_{8}		
			TDH			= {9}	TDH	

SSPMA FIGURE "D"



Friction factors for pipe fittings in terms of equivalent feet of straight pipe

Nominal Pipe Size	90 Deg. Elbow	45 Deg. Elbow	Tee (Thru-flow)	Tee Branch flow	Swing v Check Valve	Gate Valve
2"	5.2	2.8	3.5	10.3	17.2	1.4
2-1/2"	6.2	3.3	4.1	12.3	20.6	1.7
3"	7.7	4.1	5.1	15.3	25.5	2

Total fixtu	ıre units from Fig. "A" w	ork sheet		55	_{1}				
GPM requ	uirements from Fig. "B"	30	_{2}	GPM	30				
Pipe Size				2"	_{3}				
Friction fa	actors from Fig. "D"	Factor	Qty.	Total					
	90 Deg. bends	5.2	3	15.6					
	45 Deg. bends		0	0					
	Tee (thru-flow)		0	0					
	Tee (branch flow)		0	0					
	Swing check valve	17.2	1	17.2					
	Gate valve	1.4	1	1.4					
	Disch. Pipe length			200	{4}				
	Systems' total feet o	f piping		234.2	{ 5}				
Friction he	ead per / 100' of pipe fro	om Fig. "E"			_{6}				
•	by the number of 100' instem piping to determin			Friction H Static He			_{7} _{8}		
. 10001				TDH			= - {9}	TDH	

Total Dynamic Head (TDH)



- * Determine discharge piping size {3}.
- * Determine length of discharge piping {4}.
- * List all fittings and multiply by their factor. Add to length of discharge piping {4} to determine systems total feet of piping {5}.
- * Enter friction head per 100' of pipe from figure "E" {6}.

SSPMA FIGURE "E"

Friction head in feet per 100' of Schedule 40 pipe

	2'	1	2-1	/2"	3"	
GPM	Plastic	Steel	Plastic	Steel	Plastic	Steel
20	0.9	0.9				
25	1.3	1.3				
30	1.8	1.8	0.6	0.8		
35	2.4	2.4	0.8	1		
40	3.1	3.1	1	1.3		
45	3.8	3.8	1.3	1.6	0.5	0.6
50	4.7	4.7	1.6	1.9	0.7	0.7
60	6.5	6.6	2.2	2.7	0.9	0.9
70	8.6	8.8	2.9	3.6	1.2	1.2
80	11.1	11.4	3.7	4.6	1.5	1.6
90	13.8	14.3	4.6	5.8	1.9	2
100	16.8	17.5	5.6	7.1	2.3	2.4
125			8.3	10.9	3.6	3.6
150			12	15.5	4.9	5.1
175			16.4	20.9	6.4	6.9
200					8.4	8.9
225					10.5	11.2

Total fixture units from Fig. "A"	work sheet	55{1}					
GPM requirements from Fig. "B	GPM requirements from Fig. "B"						
Pipe Size			{3}				
Friction factors from Fig. "D"	Factor	Qty.	Total				
90 Deg. bends	5.2	3	15.6				
45 Deg. bends		0	0				
Tee (thru-flow)		0	0				
Tee (branch flow)		0	0				
Swing check valve	17.2	1	17.2				
Gate valve	1.4	1	1.4				
Disch. Pipe length			200 {4}				
Systemal total fact	of piping		(5)				
Systems' total feet	or piping		234.2 {5}				
Friction head per / 100' of pipe f	rom Fig. "E"		. 1.8 {6}				
Multiplied by the number of 100 of total system piping to determ Head.			Friction Head Static Head	{7} {8}			
i iodu.			TDH	{9}	TDH		

Total Dynamic Head (TDH)



* Multiply friction head per / 100' of pipe by the number of 100' increments from systems total feet of piping {7}.

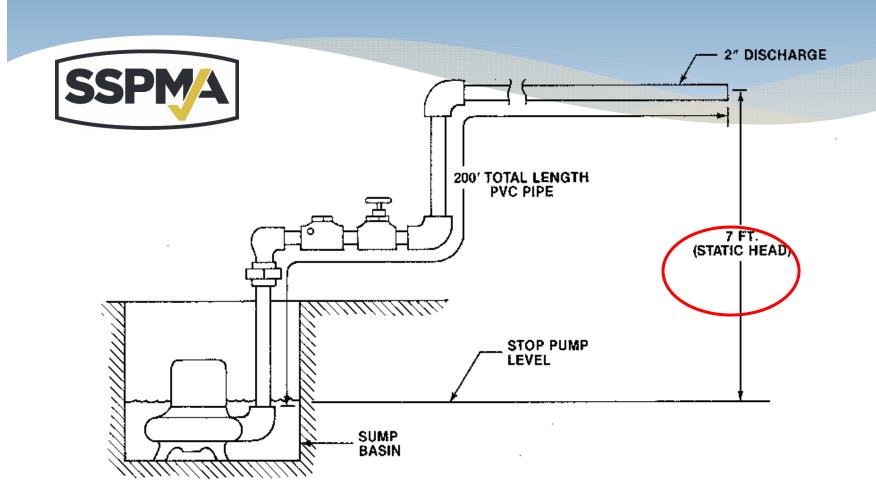
Total fixture units from Fig. "A" w	55 {1}				
GPM requirements from Fig. "B"				30 {2}	GPM 30
Pipe Size			{2"{{3}}		
Friction factors from Fig. "D"	Factor	Qty.	Total		
90 Deg. bends	5.2	3	15.6		
45 Deg. bends		0	0		
Tee (thru-flow)		0	0		
Tee (branch flow)		0	0		
Swing check valve	17.2	1	17.2		
Gate valve	1.4	1	1.4		
Disch. Pipe length			200 {4}		
Systems' total feet of	f piping		234.2 {5}		
Friction head per / 100' of pipe from	om Fig. "E"		. 1.8 {6}		
Multiplied by the number of 100' of total system piping to determine Head.			Friction Head Static Head	4.22 {7} {8}	
i icau.			TDH	{9}	TDH

Total Dynamic Head (TDH)



- * Multiply friction head per / 100' of pipe by the number of 100' increments from systems total feet of piping {7}.
- * Enter system static head {8}.

SSPMA FIGURE "C"

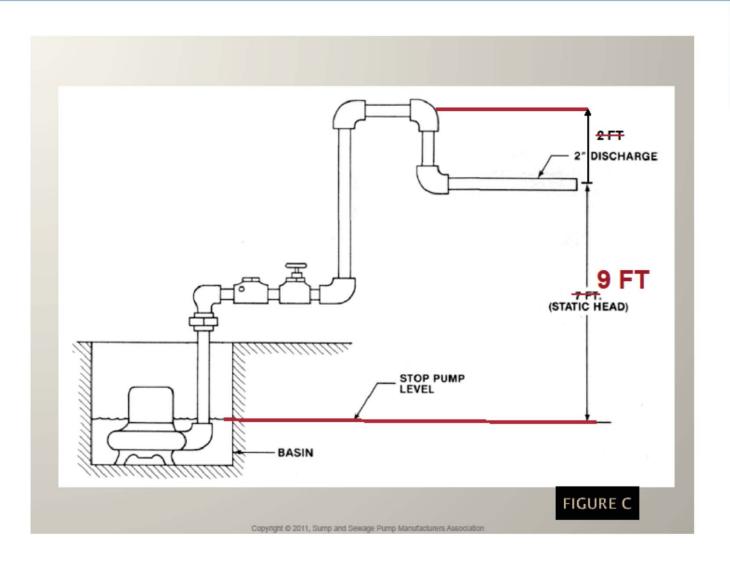


Total fixto	ure units from Fig. "A" w	ork sheet	55{1}					
GPM req	uirements from Fig. "B"	30 {2}	GPM	30				
Pipe Size	·			2"	_{3}			
Friction fa	actors from Fig. "D"	Factor	Qty.	Total				
	90 Deg. bends	5.2	3	15.6				
	45 Deg. bends		0	0				
	Tee (thru-flow)		0	0				
	Tee (branch flow)		0	0				
	Swing check valve	17.2	1	17.2				
	Gate valve	1.4	1	1.4				
	Disch. Pipe length			200	{4}			
	Systems' total feet o	f piping		234.2	{5 }			
Friction h	ead per / 100' of pipe fro	om Fig. "E"		. 1.8	_{6}			
•	d by the number of 100' in stem piping to determing			Friction H Static He		4.22 {7} 7 {8}		
				TDH		{9}	TDH	

CAUTION!



The point of discharge MAY NOT be the highest point in the piping system. A pump must be selected that has a shut-off head greater than the highest point in the pipe system.



Total Dynamic Head (TDH)



- * Multiply friction head per / 100' of pipe by the number of 100' increments from systems total feet of piping {7}.
- * Enter system static head {8}.
- * Add friction head and static head to determine TDH {9}.

System Requirements

Total fixture units from Fig. "A" work sheet	55	_{1}		
GPM requirements from Fig. "B"	30	{2}	GPM	30

Friction factors from Fig. "D"	Factor	Qty.	Total	_
90 Deg. bends	5.2	3	15.6	
45 Deg. bends		0	0	
Tee (thru-flow)		0	0	
Tee (branch flow)		0	0	
Swing check valve	17.2	1	17.2	
Gate valve	1.4	1	1.4	
Disch. Pipe length			200	{4 }
Systems' total feet of	f piping		234.2	{5 }

Friction head per / 100' of pipe from Fig. "E" 1.8 {6}

Multiplied by the number of 100' increments Friction Head 4.22 {7 of total system piping to determine Friction Static Head 7 {8 Head.

TDH

11.22 {9}

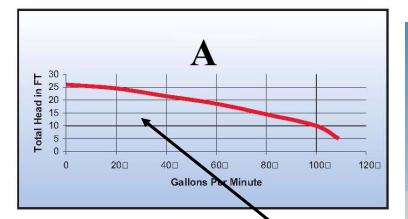
TDH

11.22

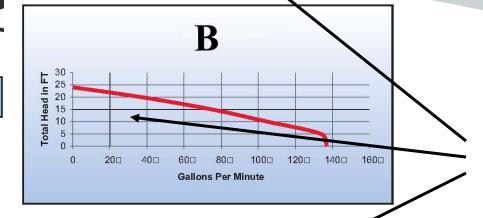
OVERSIZING THE PUMP?

- •The most efficient part of the curve is usually in the middle of the curve, away from maximum head or flow
- More horsepower or flow is not always better – especially in smaller basins
- •Short cycling may reduce the life of the pump. A longer pumping cycle will be better for pump longevity.

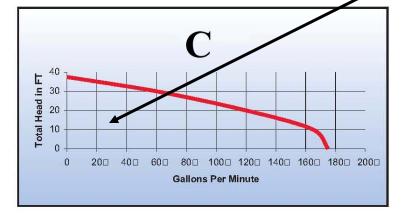




1/2HP



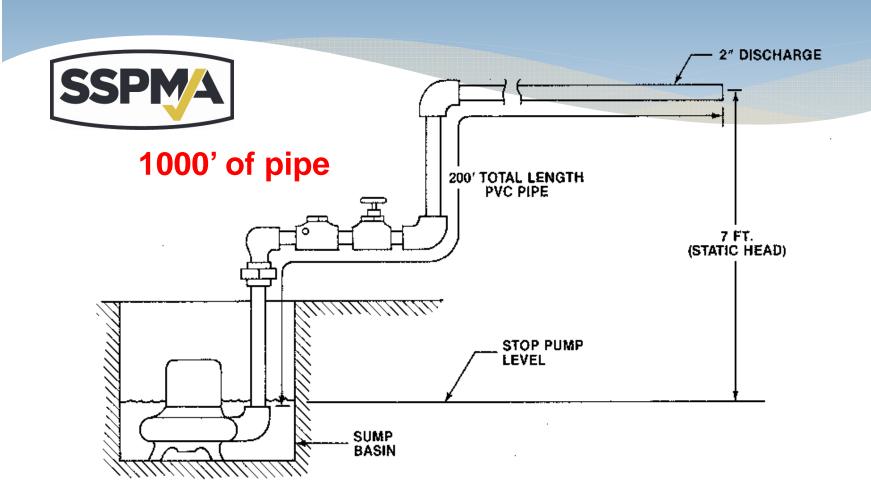
3/4HP



SSPMA FIGURE "F"

Recommended Basin Diameters								
	GPM	18"	24"	30"	36"	48"		
	2 0							
V	25							
	3 0							
	3 5							
	4 0							
	4 5							
	5 0							
	6 0							
	7 0							
	8 0							
	9 0							
	100							
	125							
	150							
	175							
	200							
	225							
	250							

SSPMA FIGURE "C"



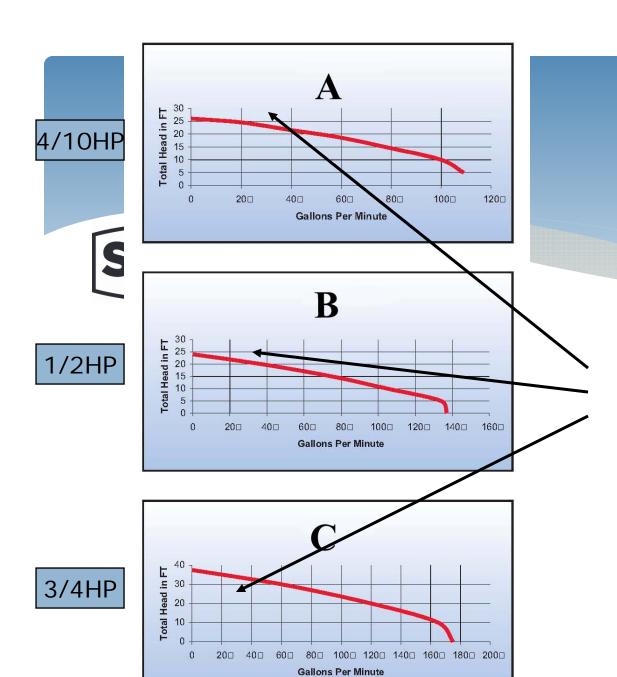
SIZING WORKSHEET System Requirements Total fixture units from Fig. "A" work sheet ___{1} GPM requirements from Fig. "B" {2} **GPM** 30 Pipe Size 2" {3} Friction factors from Fig. "D" Factor Qty. Total 90 Deg. bends 5.2 3 15.6 45 Deg. bends 0 0 Tee (thru-flow) 0 0 Tee (branch flow) 0 0 17.2 Swing check valve 17.2 1 1.4 Gate valve 1 1.4 Disch. Pipe length 1000 {4} Systems' total feet of piping {5} Friction head per / 100' of pipe from Fig. "E" 1.8 Multiplied by the number of 100' increments Friction Head of total system piping to determine Friction Static Head

TDH

TDH

Head.

			SIZIN	IG WOR	KSł	HEET	•		System Re	quirements
Total fixtur	e units from Fig. "A" w	ork sheet				····· -	55	{1}		
GPM requi	rements from Fig. "B"					···· -	30	{2}	GPM	30
Pipe Size				2"	_{3}					
Friction fac	ctors from Fig. "D"	Factor	Qty.	Total						
	90 Deg. bends	5.2	3	15.6						
	45 Deg. bends		0	0						
	Tee (thru-flow)		0	0						
	Tee (branch flow)		0	0						
	Swing check valve	17.2	1	17.2						
	Gate valve	1.4	1	1.4						
	Disch. Pipe length			1000	{4}					
	Systems' total feet o	l f piping		1034.2	{5}	—				
Friction he	ad per / 100' of pipe fro	om Fig. "E"		1.8	_ {6}	—				
•	by the number of 100' interest the stem piping to determinate.			Friction Hea		-	18.6156 7	{7} {8}	—	
				TDH		Ç	26'	3 9}	TDH	26'



Minimum Pump Capacity



2' Per Second To Carry Solids

12 GPM in 1-1/2" Pipe 21 GPM in 2" Pipe 46 GPM in 3" Pipe

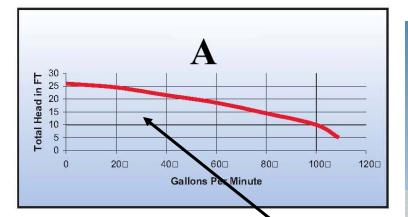
SSPMA FIGURE "E"

Friction head in feet per 100' of Schedule 40 pipe

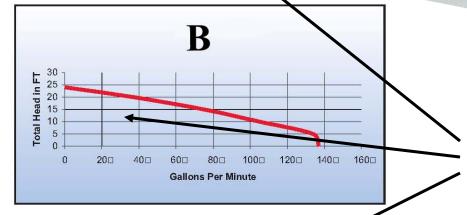
	2"		2-1	/2"	3"	
GPM	Plastic	Steel	Plastic	Steel	Plastic	Steel
20	0.9	0.9				
25	1.3	1.3				
30	1.8	1.8	0.6	0.8		
35	2.4	2.4	0.8	1		
40	3.1	3.1	1	1.3		
45	3.8	3.8	1.3	1.6	0.5	0.6
50	4.7	4.7	1.6	1.9	0.7	0.7
60	6.5	6.6	2.2	2.7	0.9	0.9
70	8.6	8.8	2.9	3.6	1.2	1.2
80	11.1	11.4	3.7	4.6	1.5	1.6
90	13.8	14.3	4.6	5.8	1.9	2
100	16.8	17.5	5.6	7.1	2.3	2.4
125			8.3	10.9	3.6	3.6
150			12	15.5	4.9	5.1
175			16.4	20.9	6.4	6.9
200					8.4	8.9
225					10.5	11.2

SIZING WORKSHEET System Requirements Total fixture units from Fig. "A" work sheet 55 {1} GPM requirements from Fig. "B" **GPM** 30 46 Pipe Size 2" {3} **Factor** Qty. Total 90 Deg. bends 5.2 3 15.6 0 45 Deg. bends 0 Tee (thru-flow) 0 0 Tee (branch flow) 0 0 17.2 Swing check valve 17.2 Gate valve 1.4 1.4 Disch. Pipe length 1000 {4} Systems' total feet of piping **1034.2** {5} Friction head per / 100' of pipe from Fig. "E" 5.17 Multiplied by the number of 100' increments Friction Head 18.0150 {7} of total system piping to determine Friction Static Head Head. TDH {9} **TDH** 26' 12.17

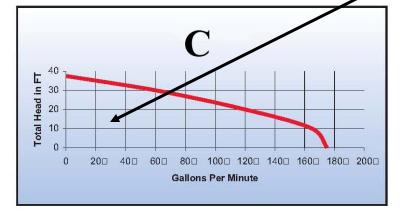




1/2HP



3/4HP



Congratulations!



